

Full Length Research Paper

Lattice Boltzmann simulation of the two-dimensional Poiseuille-Rayleigh-Benard flows instability

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A numerical method based on the lattice Boltzmann equation (LBE) is developed in two dimensions to solve the equations of conservation of energy and momentum of a Poiseuille-Rayleigh-Benard (PRB) mixed-flow. The configuration considered in this work is a channel heated from below, cooled from the top and crossed by a fluid ($Pr = 1$). The study is conducted for a range of Rayleigh numbers ($0 < Ra < 5000$) and Reynolds ($0 < Re < 500$). For $Re = 0$ and Ra exceeds the critical value (1707.76), the Rayleigh-Benard (RB) mixed-flow appears. However, for Re values other than 0, the transition from Poiseuille flow in a cellular flow is obtained for the largest critical Ra (in limited area) and characteristics of cells depend on the intensity of the flow at the entrance of the channel.

Key words: Poiseuille-Rayleigh-Benard flow, Lattice Boltzmann equation (LBE), horizontal rectangular channel.

INTRODUCTION

The Poiseuille-Rayleigh-Benard (PRB) mixed-flows are flows subjected to a longitudinal pressure gradient in horizontal rectangular channels (Figure 1) which are heated from below and cooled from above. The Reynolds numbers are sufficiently low (≤ 500) not to trigger shear instability. The conductive state, characterized by a thermally stratified parallel flow, is stable to temperature differences which are sufficiently low (Mbane et al., 2007; Miladinova et al., 2004). Beyond a threshold defined by a critical Rayleigh number located in the vicinity of 1708, the conductive state becomes unstable and the thermoconvective structures appear. It is known that in a rectangular channel, the flow changes into a row of counter rotating vortices, indicating the Reynolds numbers are sufficiently large and moving in the direction of flow under the influence of longitudinal pressure gradient (Dondlinger et al., 2003).

Clever and Busse (1991) numerically determined the temporal linear stability of flow in a structured longitudinal roll between two infinite plates. They show that in an area of the ($R_{\text{eynolds}} R_{\text{ayleigh}}$)-plane this primary instability becomes unstable with respect to transverse perturbations and passes a flow form of stationary rolls

independent of the longitudinal component in a set of sinuous unsteady rolls.

The Poiseuille-Rayleigh-Benard (PRB) mixed-flows represent a vast subject and is an active topic of research, both for industrial problems and for numerous applications in wide array of different fields, ranging from cosmetics, food processing, oil industry and to natural settings such as lava mud and biology (blood, mucus). This configuration is rich in terms of thermoconvective flow structures (transverse, parallel, oblique, tortuous, varicose rolls form, etc.) and is a typical problem in analysis of stability and control runoff from a both sides share has applications in the study of chemical vapour deposition (CVD). Hydrodynamical stability studies are essential to understand the transition between stable and unstable flows, because flow instability is often associated with an increase in heat transfer.

The lattice Boltzmann methods (LB) have emerged as a powerful technique for the computational modelling of wide variety of complex fluid flow problems including single phase flow in complex geometries. These methods naturally accommodate a variety of boundary conditions such as the wetting effects at a fluid-solid interface. The discrete Boltzmann methods serve as an ideal mesoscopic approach that bridges microscopic phenomena with the continuum macroscopic equation. In this respect, the aim of our work is to use for the first time a Lattice Boltzmann Model (LBM) built from simple and parallelizable

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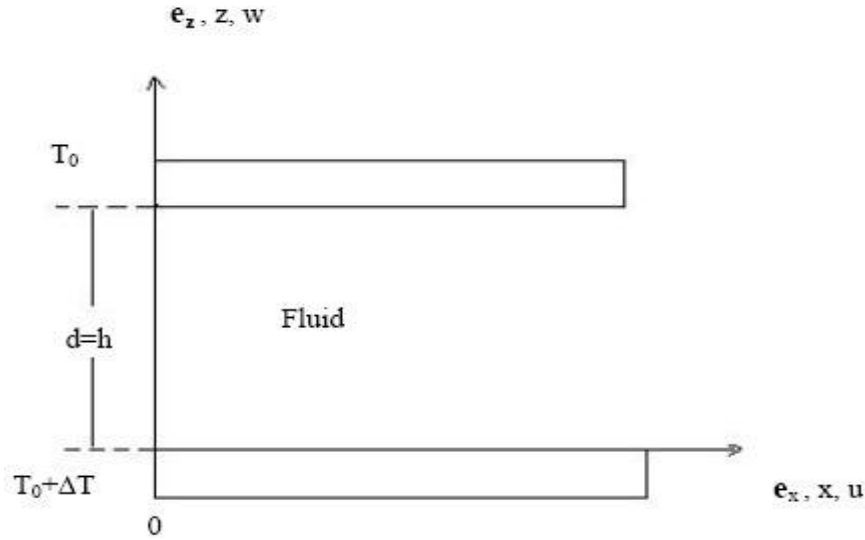


Figure 1. The P-R-B flow's horizontal channel.

algorithms, to solve the Navier Stokes equations (Buick et al., 2000; Ginzburg, 2001; Ginzburg and Steiner, 2002) and simulate the Poiseuille-Rayleigh-Benard flows (Figure 1).

BASIC THEORY OF LATTICE BOLTZMANN EQUATION

The lattice Boltzmann equation (LBE) is often written in the following form (Succi et al., 1991)

$$\tilde{N}_i(\mathbf{r}, t) = N_i(\mathbf{r}, t) + \sum_{j=0}^{b_m} A_{ij} [N_j(\mathbf{r}, t) - N_j^{eq}(\mathbf{r}, t)] + T_p^*(\mathbf{C}_i, \mathbf{F}) \tag{1a}$$

$$\tilde{N}_i(\mathbf{r}, t) = N_i(\mathbf{r} + \mathbf{c}_i \cdot \Delta t, t + \Delta t), \quad i = 0, \dots, b_m \tag{1b}$$

Where N_i is the population of the particle moving with D -dimensional velocity \mathbf{c}_i (\mathbf{c}_0 is the zero vector), A is the collision matrix, \mathbf{F} is an external force; weight coefficient T_p^* depends on the discrete velocity set \mathbf{c}_i , and the index p is equal to c_i^2 , ($c_i^2 = \mathbf{c}_i^2$). Equilibrium function N^{eq} is introduced by the hydrodynamics adopted Equations (Qian et al., 1992) and the coefficients T_p^* are given in Table 1. They satisfy the following equations

$$\sum_{i=1}^{b_m} T_p^* \mathbf{c}_{i\alpha}^2 = 1, \quad \forall \alpha = 1, \dots, D \quad \text{and} \quad T_0^* = 3 - \sum_{p \neq 0} T_p^* \tag{2}$$

There are two essential steps in Equation (1a): *collision* (a) and *propagation* (b). Density ρ and momentum \mathbf{j} are defined as

$$\rho(\mathbf{r}, t) = \sum_{i=0}^{b_m} N_i(\mathbf{r}, t) \tag{3a}$$

$$\mathbf{j}(\mathbf{r}, t) = \mathbf{J} + \frac{1}{2} \mathbf{F}, \quad \mathbf{J} = \sum_{i=1}^{b_m} N_i(\mathbf{r}, t) \cdot \mathbf{c}_i \tag{3b}$$

The reason of modification of the momentum as a function of force was studied in detail by Buick and Greated (2000); Ginzburg and d’Humières (2002). The mass and momentum conservation laws impose the following conditions on the collision matrix A

$$A \cdot \mathbf{1} = A, \quad C_\alpha = 0, \quad \forall \alpha = 1, \dots, D \tag{4}$$

Where $\mathbf{1} = \{1, \dots, 1\}$, and the (b_m+1) -vector C_α is built from the components of the $(b_m + 1)$ population velocities in direction α .

The collision matrix is determined by the choice of its non-zero eigenvalues and the corresponding eigenvectors. To satisfy the linear stability conditions (Higuera et al., 1989), the non-zero eigenvalues must lie in the interval $-2, 0$. Mass vector $\mathbf{1}$ and the vectors C_α are

Table 1. Equilibrium weights T_p^* and r_p^*

Model	T_0^*	T_1^*	T_2^*	T_3^*	r_0^*	r_1^*	r_2^*	r_3^*
D2Q9	$\frac{4}{3}$	$\frac{1}{3}$	$\frac{1}{12}$	–	$\frac{3-5C_\alpha^2}{3}$	$\frac{C_\alpha^2}{3}$	$\frac{C_\alpha^2}{12}$	–
D3Q15	$\frac{2}{3}$	$\frac{1}{3}$	–	$\frac{1}{24}$	$\frac{3-7C_\alpha^2}{3}$	$\frac{C_\alpha^2}{3}$	–	$\frac{C_\alpha^2}{12}$

the eigenvectors associated with the zero eigenvalues. They are the conserved modes in the model.

Let $\{e_k\}$, $k = 0, \dots, b_m$ denote the orthonormal basis in momentum space, constructed as the polynomials of the vectors $C\alpha$. Let us assume that this basis represents the set of the eigenvectors of the matrix A , associated with the eigenvalues $\{\lambda_k\}$. The projection of Equation (1a) on this basis gives

$$\tilde{N}_i(\mathbf{r}, t) = N_i(\mathbf{r}, t) + \sum_{j=0}^{b_m} \lambda_k (\mathbf{N} - \mathbf{N}^{eq}, \mathbf{e}_k) e_{ki} + T_p^*(\mathbf{c}_i, \mathbf{F}) \quad (5a)$$

$$\tilde{N}_i(\mathbf{r}, t) = N_i(\mathbf{r} + \mathbf{C}_i \cdot \Delta t, t + \Delta t), \quad i = 0, \dots, b_m \quad (5b)$$

Note that Equation (5a) replaces the explicit use of the collision matrix A . The eigenvalues can also be easily adjusted during computations, if necessary, providing that they satisfy the stability constraints. When all non-zero eigenvalues $\{\lambda_k\}$ are set to be equal to $-1/\tau$, equation (5a) reduces to the lattice Bhatnagar-Gross-Krook model (LBGKM)

$$N_i(\mathbf{r} + \mathbf{c}_i \cdot \Delta t, t + \Delta t) = N_i(\mathbf{r}, t) - \frac{1}{\tau} (N_i - N_i^{eq}) + T_p^*(\mathbf{c}_i, \mathbf{F}) \quad (6)$$

Where τ is the relaxation time.

MATERIALS AND METHODS

D2Q9 lattice (Figure 2) is adopted to solve 2D fluid flow and heat transfer problem by using two distribution functions approach.

The method used is to determine the solution of the following equation deduced from the LBGK model (6)

$$f_i(\mathbf{x} + \mathbf{c}_i \cdot \Delta t, t + \Delta t) - f_i(\mathbf{x}, t) = \Omega_i \quad (7)$$

Where f_i is the distribution function of the particle moving with D-dimensional velocity \mathbf{C}_i . The principle of this approximation is based on the fact that the collision term Ω_i representing the rate

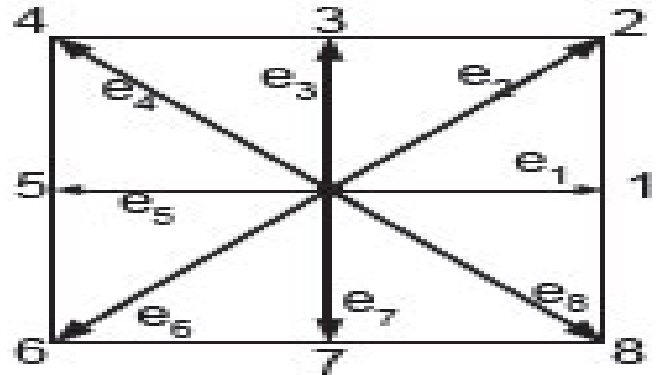


Figure 2. Orthogonal basis vectors for D2Q9 model.

of change of the particle distribution due to collision may be replaced by a linear approach

$$\Omega_i = - \frac{f_i - f_i^{eq}}{\tau} + \delta_i F_i \quad (8)$$

Where τ is the relaxation time that controls the rate of approach to equilibrium and f_i^{eq} the distribution function at equilibrium depends on the local hydrodynamic properties. $\delta_i F_i$ is an external force. The function f_i^{eq} defined below is used as a distribution function at equilibrium,

$$f_i^{eq} = \omega_i \rho \left[1 + 3 \frac{\mathbf{c}_i \cdot \mathbf{u}}{c^2} + \frac{9}{2} \frac{(\mathbf{c}_i \cdot \mathbf{u})^2}{c^4} - \frac{3}{2} \frac{\mathbf{u} \cdot \mathbf{u}}{c^2} \right] \quad (9)$$

\mathbf{u} and ρ are the respective values of the macroscopic velocity and density. ω_i are the statistic weights according to each direction of the Boltzmann's lattice. Macroscopic hydrodynamic quantities are determined in momentum space

$$\rho(\mathbf{x}, t) = \sum_i f_i(\mathbf{x}, t) \quad (10)$$

$$\rho \mathbf{u}(\mathbf{x}, t) = \sum_i \mathbf{c}_i f_i(\mathbf{x}, t) \quad (11)$$

The viscosity and thermal diffusivity are respectively related to the dimensionless relaxation times by the formulas

$$\nu = (\tau_\nu - \frac{1}{2})c_s^2 \cdot \delta t \tag{12}$$

$$\alpha = \frac{1}{3}(\tau_T - \frac{1}{2})c_s^2 \cdot \delta t \tag{13}$$

Where C_s is the speed of sound in the lattice and δt the time steps.

The time evolution of the particle temperature distribution function satisfies the following lattice Bhatnagar-Gross-Krook (LBGK) equation

$$g_i(\mathbf{x} + \mathbf{c}_i \Delta t, t + \Delta t) - g_i(\mathbf{x}, t) = -\frac{1}{\tau_T} (g_i(\mathbf{x}, t) - g_i^{eq}(\mathbf{x}, t)) \tag{14}$$

g_i and τ_T represent the distribution function of energy and the dimensionless relaxation time for the thermal field, respectively. A macroscopic quantity such as the temperature of each fluid component is obtained by taking suitable moment sums of g_i

$$\rho \cdot \mathcal{E} = \sum_i g_i \tag{15}$$

\mathcal{E} represents the energy.

The above formalism leads to velocity and thermal fields that are solutions of the Navier-Stokes equations.

RESULTS AND DISCUSSION

Validation of the LBGK model

The model was validated by considering a differentially heated square cavity containing a fluid whose Prandtl number was set at 0.71 ($Pr = 0.71$). The simulations were performed for different values of Rayleigh number ranging from 10^3 to 10^6 . The physical quantities such as speed (u_{max}), cinematic viscosity (ν_{max}) and Nusselt number (Nu) are calculated by the model and compared to their reference values (Table 2).

Numerical results are in good agreement with results obtained by de Vahl Davis (1983) as shown in Figures 3 a - c. Differences between reference values and values estimated by the model are sufficiently low ($\leq 0.48\%$). Profiles of velocity and temperature fields presented by the model were also in good agreement with those of previous fields.

Numerical simulations

The LBGK method is applied to a horizontal channel of rectangular cavity whose width is four times greater than

the height (expansion ratio equal to 4). In the absence of jet, the convective flow within the channel is Rayleigh-Benard. It is triggered when the Rayleigh number Ra exceeds the critical value $Rac = 1707$, with the appearance of four contra rotative cells (Figure 4a). The thermal field observed at this particular time is shown in Figure 4b.

For low values of Reynolds number Re ($Re < 0.1$), the jet has no significant effect on the appearance of convective instabilities. However, the isotherms are distorted by the intensity of flow inside the channel. Convective transfer on the surface of the horizontal walls is improved. Increasing the Reynolds number Re , delays the appearance of convective instability within the channel. Indeed, for $Re = 10$, the convective rolls appear when $Rac = 8500$ (Figures 5).

Convective rolls visible in Figures 5 are not stationary and moving under the influence of flow along the channel that leads to a periodic variation of macroscopic variables. Figure 6 shows the variation with time of the maximum speed on the vertical plane. This speed is very low values in Poiseuille flow. The appearance of convective cells is indicated by a significant increase in maximum speed: this means an improvement in heat transfer through the fluid.

One can observe from Figure 6 that the intensity of the maximum velocity decreases with time. In other words the intensity of the jet at the entrance of the channel delays the appearance of convective cells. LBGK model may also help visualize the temporal variations of other flow characteristics such as the Nusselt number for a given couple of values of Reynolds and Rayleigh (Figure 7).

Conclusion

This paper presents a review of possibilities offered by the LBGK model in the study of a fluid ($Pr = 1$) subjected to a longitudinal pressure gradient in horizontal rectangular channels which are heated from below and cooled from above. Unlike conventional methods based on macroscopic continuum equations, the LBGKM uses a microscopic equation, that is, the Boltzmann equation, to determine macroscopic fluid dynamics. The LBGKM is flexible, has broad applicability that is, cooling of electronic components and may be easily adapted for parallel computing. The challenge for this study is to acquire a better understanding of such flows simply by varying the Reynolds number or any other number or parameter that we seek to know the influence on the flow regime. The Lattice Boltzmann methods are currently in a state of evolution as the models become better understood and are corrected for various deficiencies. Results obtained in this work demonstrate the effectiveness of the Boltzmann methods and suggest a next step in terms of simulation of non axisymmetric stokes flow between concentric cones.

Table 2. Model and reference data (maximum velocity, maximum viscosity and Nusselt number) for different values of Rayleigh ranging from 10^3 to 10^6 .

Ra	U_{max}			v_{max}			Nu		
	Model	Reference	% error	Model	Reference	% error	Model	Reference	% error
10^3	3.699	3.697	0.05	3.650	3.649	0.027	1.116	1.118	0.18
10^4	19.620	19.617	0.015	16.167	16.178	0.067	2.245	2.243	0.09
10^5	68.68	68.59	0.13	33.68	34.73	0.03	4.521	4.519	0.04
10^6	220.418	219.36	0.48	64.763	64.63	0.205	8.814	8.800	0.16

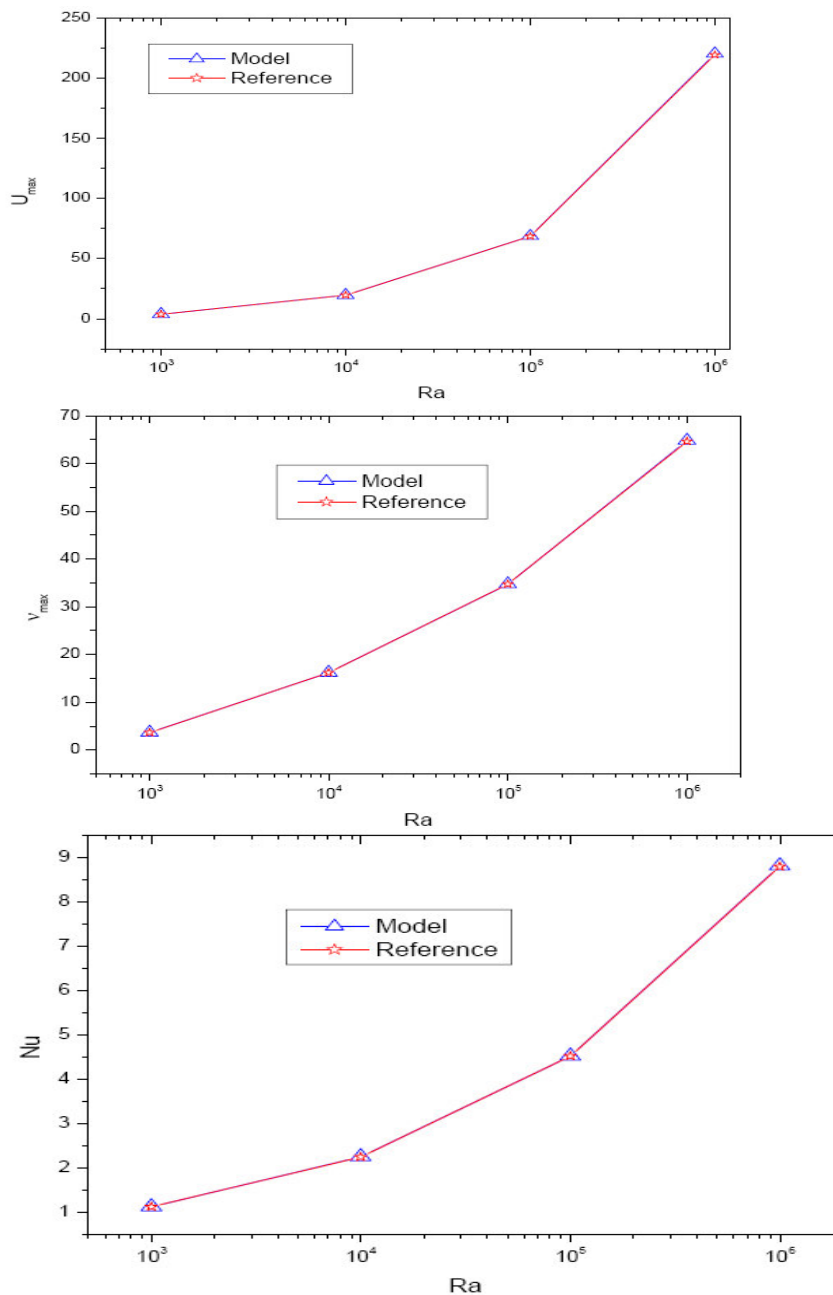


Figure 3. Comparison between predicted and reference values of the maximum velocity, viscosity and Nusselt number.

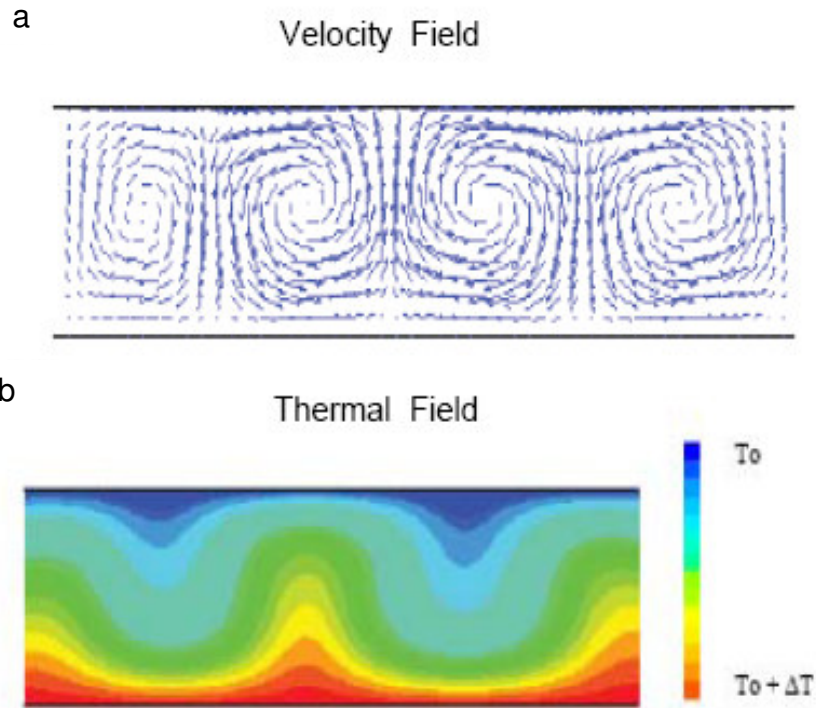


Figure 4. Velocity field (a) and thermal field (b) predicted by LBGK model for $Re = 0$ and $Ra = 1750$.

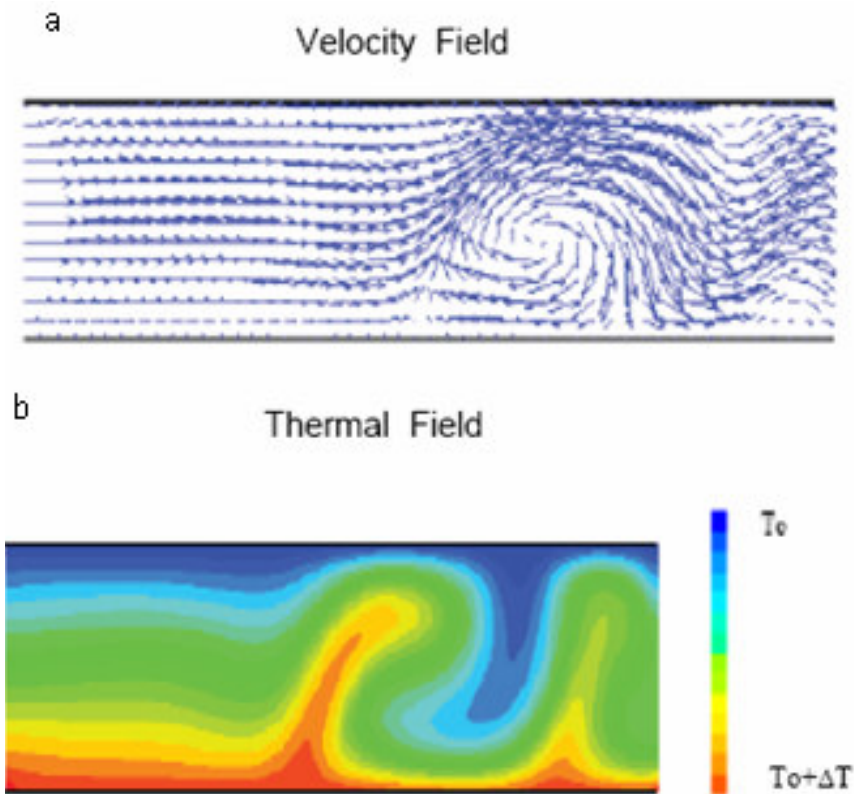


Figure 5. Velocity field (a) and thermal field (b) predicted by LBGK model for $Re = 10$ and $Ra = 8500$.

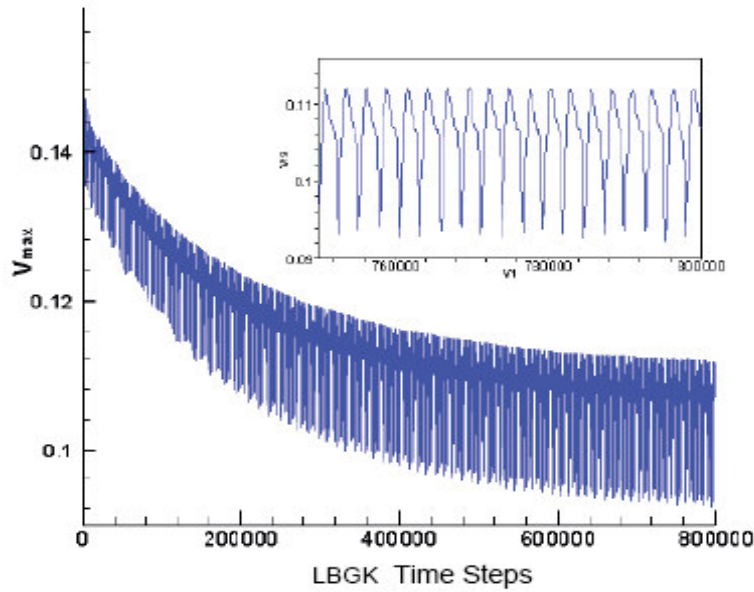


Figure 6. Temporal evolution of the predicted maximum velocity for $Re = 10$ and $Ra = 8500$.

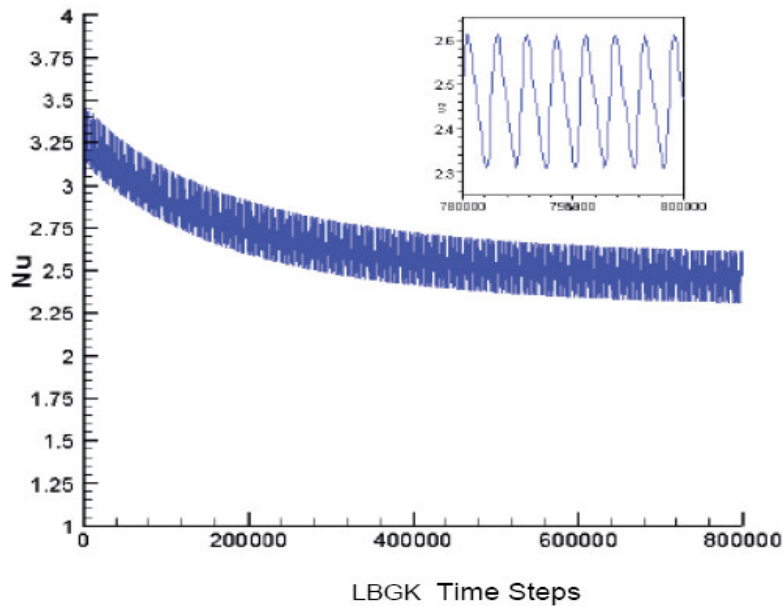


Figure 7. Temporal evolution of the predicted Nusselt number for $Re = 10$ and $Ra = 8500$.

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